

DOSE THE RIGHT AMOUNT OF CHEMICALS

By K.K.PARTHIBAN, Boiler Consultant

Venus Energy Audit System

Email ID:parthi2006@gmail.com / venus.energy@gmail.com

Recently I had come across a case of erratic chemical dosing and boiler water pH dipping below 7.5. It can happen on many occasions.

1. When we base blow down on silica in steam, we may not be able to make up the phosphate level suitably.
2. When we try intermittent blow down, there is a heavy drain of boiler water & phosphate. We will not be able to make up for the drained phosphate with regular dosage rates of chemicals.
3. During start up and during very high load variations, chemical make up may not be sufficient.
4. When there is a time lag between analysis and dosage setting, the chemical level would vary heavily.
5. When the deaerator water temperature is low, the boiler water pH may get upset.
6. When the condensate contamination is possible, then again we may not be able to maintain boiler water chemistry.

When there are several reasons for the boiler water chemistry upset, we need to know how much we need to dose to bring back normalcy. We need to know the fundamentals of chemical dosing calculations. The calculation sheet given in this paper briefs how to calculate the chemical requirement. Instead of looking at the water sample results and then correcting the dosage we can decide how much is to be dosed. If the chemical dosing pump is a limitation, then % dilution can be changed for some time to bring back to normalcy. This calculation is for the boilers where the basic chemicals are used. The calculations will however be similar for proprietary chemical as well. Knowing the water volume in boiler is necessary to decide the dump dosage of chemical during upsets.

WATCH THE EFFECTIVENESS OF CHEMICAL DOSING!

Many boiler users leave the water chemistry management to chemical supplier. The dosage practices are decided by the chemical suppliers. But then how to ensure that the chemicals are protecting the boiler? The best way is to inspect the wetted surfaces of the boiler. In Shell type boiler it is rather easy to see the tubes for scale or pitting. But in water tube boiler, the steam drum only speaks. The best way is to open the steam drum and take a wipe of the drum internal surface with your palm. Generally the water tube boiler is fed with well treated water. Hence scale related problems are not experienced. However the corrosion of economizer / boiler could be a serious problem. The presence of loose reddish powder indicates the boiler is corroding. Presence of grey powder indicates the economizer / pre-boiler system corrosion.

LP / HP CHEMICAL DOSING CALCULATIONS**INPUTS**

| | | |
|--|-------|-------------|
| Steam generation rate Nett = | 10000 | kg / hr |
| TDS in feed water = | 0.1 | ppm |
| TDS permitted in boiler water = | 25 | ppm |
| Oxygen in feed water = | 0.02 | ppm |
| Oxygen permitted in feed water = | 0.002 | ppm |
| Residual phosphate level in boiler water = | 4 | ppm |
| Concentration of phosphate solution = | 0.3 | gm / 100 ml |
| Residual sulphite in feed water = | 15 | ppm |
| Concentration of sulphite solution = | 0.04 | gm / 100 ml |
| Residual Hydrazine in Feed water = | 0.02 | ppm |
| Concentration of hydrazine solution = | 35 | % |

HP CHEMICAL DOSING CALCULATION

| | |
|---|----------------------------------|
| Chemical Dosed in HP Dosing System = | TRI SODIUM PHOSPHATE |
| Maximum steam generation capacity of boiler = | 10000 kg / hr |
| TDS in feedwater = | 0.1 ppm |
| TDS permitted in Boiler water = | 25 ppm |
| Percentage blow down = | $100 \times 0.1 / (25 - 0.1)$ |
| | = 0.4 % |
| Actual blow down rate = | $10000 \times 0.4 / 100$ kg / hr |
| | = 40 kg/hr |
| Recommended phosphate ppm in boiler water = | 4 ppm |
| Loss of phosphate in blow down water = | $4 \times 40 / 1000$ g / hr |
| | = 0.16 gm / hr |
| Loss of TSP in blow down water = | 0.16×4 |
| | = 0.64 gm/h |
| Tri sodium phosphate consumption per day = | $0.64 \times 24 / 1000$ kg / day |
| | = 0.01536 kg / day |

LP CHEMICAL DOSING CALCULATION

| | |
|---|--|
| Chemical dosed = | SODIUM SULPHITE |
| Maximum steam generation capacity of boiler = | 10000 kg / hr |
| Oxygen in feedwater = | 0.02 ppm |
| Required oxygen level in feed water = | 0.002 ppm |
| Oxygen to be removed = | $0.02 - 0.002 \times 10000 \times 0.000001$ kg / hr |
| | = 0.00018 kg / hr |
| Oxygen to be removed in moles per hr = | $0.00018 / 32$ |
| | = 0.000005625 kg / hr |
| Sulphite required in moles per hr = | 2×0.000005625 |
| | = 1E-05 |
| Sulphite required in gms per hr = | molecular wt (Na ₂ SO ₃)x moles/h |
| | = $\{1000 \times [(2 \times 23) + (32) + (3 \times 16)]\} \times 0.00001125$ gm/hr |
| | = 1.4175 gm / hr |
| Concentration of sodium sulphite solution = | 0.04 gm / 100 ml |
| Rate of dosing = | $100 \times 1.4175 / 0.04$ ml / hr |
| | = 3543.75 ml / hr |
| Sodium sulphite consumption per day = | $(1.4175 \times (24 / 1000))$ kg / day |

$$= \mathbf{0.034 \text{ Kg / Day}}$$

LP CHEMICAL DOSING CALCULATION

| | | |
|--|---|----------------------------|
| Chemical dosed | = | HYDRAZINE |
| Maximum steam generation capacity of boiler | = | 10000 kg / hr |
| Oxygen in feedwater after deaeration @105 deg C | = | 0.02 ppm |
| Required oxygen level in feed water | = | 0.002 ppm |
| Oxygen to be removed | = | 0.02 - 0.002 ppm |
| | = | 0.018 ppm |
| Hydrazine reqd (30 times depending on reaction kinetics) | = | 30 x 0.018 ppm |
| | = | 0.54 ppm |
| Residual hydrazine to be kept | = | 0.02ppm |
| Total hydrazine required | = | 0.54 + 0.02 ppm |
| | = | 0.56 ppm |
| Total hydrazine required in kg/kg of evaporation | = | 0.56 x 0.000001 kg / kg |
| | = | 0.00000056 kg / kg |
| Hydrazine required per hour | = | 10000 x 0.00000056 kg / hr |
| | = | 0.0056 kg / hr |
| Concentration of hydrazine solution | = | 35% |
| Hydrazine to be dosed @35% conc | = | 0.0056x100 / 35 kg / hr |
| | = | 0.016kg / hr |
| Hydrazine consumption per day | = | 0.01600x 24 kg / day |
| | = | 0.384 kg / day |